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Original article

Heterogeneous activation of peroxymonosulfate by recyclable magnetic CuO/Fe₃O₄ nanosheets for efficient degradation of organic pollutants

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ABSTRACT

In this work, recyclable magnetic CuO/Fe₃O₄ nanosheets were successfully synthesized via a simple continuous precipitation method, which can effectively activate peroxymonosulfate (PMS) to decompose organic pollutants. The properties of CuO/Fe₃O₄ nanosheets were measured by a series of characterization techniques. CuO/Fe₃O₄ composites showed highly effectiveness for PMS activation to degrade methylene blue (MB), and several influencing factors were investigated, such as initial pH, catalyst dosage, PMS concentration and reaction temperature. Although CuO/Fe₃O₄/PMS system exhibited effectiveness for MB degradation in a wide pH range, the natural pH value was the best. The increase in reaction temperature is favorable for MB degradation, and the activation energy was calculated as 40.34 kJ/mol. Quenching experiments and electron spin resonance (ESR) analysis proved that ·OH, SO₄⁻ and ¹O₂ were generated in the CuO/Fe₃O₄/PMS system, and SO₄⁻ and ¹O₂ played the dominant role. Moreover, CuO/Fe₃O₄ remained good activity and stability after being recycled five times. In addition, the complete degradation of methylene orange (MO) and tetracycline hydrochloride (TC), and MB degradation in tap water and lake water further confirmed the wide applicability of the CuO/Fe₃O₄/PMS system. These results exhibited that CuO/Fe₃O₄/PMS system has great advantages of high removal efficiency, reusability and wide applicability, demonstrating its potential environmental application in the treatment of organic wastewater. © 2023 The Author(s). Published by Elsevier B.V. on behalf of King Saud University. This is an open access article under the CC BY-NC-ND license (<http://creativecommons.org/licenses/by-nc-nd/4.0/>).

1. Introduction

Usually, biological processes may be the first choice in the wastewater treatment, because of the effectiveness and cost-effectiveness (Liu et al., 2022). However, conventional biological processes cannot effectively remove nonbiodegradable organic pollutants. So some new advanced oxidation processes (AOPs) have been developed to decompose the nonbiodegradable pollutants (Nguyen et al., 2020; Liu et al., 2023). Among them, sulfate radical (SO₄⁻) based advanced oxidation processes (SR-AOPs) have received increased attention (Li et al., 2022; Zhu et al., 2023; Zhang et al., 2020). SO₄⁻ has the higher oxidation potential and longer half-life than that of hydroxyl radical (·OH). Compared with H₂O₂, persulfate, including peroxymonosulfate (PMS) and perox-

odisulfate (PDS), has lots of advantages, such as lower cost, higher security, easier storage and transportation.

PMS is an asymmetric structure peroxide, which can be activated by carbon-based materials (Wang et al., 2023) transition metals (Wang et al., 2023), UV radiation (Guerra-Rodriguez et al., 2021); heat (Yin et al., 2022), ultrasound (Gujar et al., 2023); microwaves (Qi et al., 2017). Transition metal ions were used to activate PMS for the degradation of organic pollutants (Wang et al., 2023; Song et al., 2022; Mohammed Al-Balawi et al., 2023). But there are some insurmountable drawbacks for the homogeneous phase of transition metal ions; such as the high pH dependence, unrecyclable flaw. Metal oxides as heterogeneous catalysts can overcome the above drawbacks (Nguyen et al., 2023; Liu et al., 2023). Therefore, metal oxides have been intensively developed for PMS activation. For example, magnetic CoFe₂O₄ nanocrystals were prepared to activate PMS for the degradation of chloramphenicol (Yang et al., 2021) and for disinfection in different wastewater matrices (Rodriguez-Chueca et al., 2020). Nano-MoO₂ exhibited excellent performance in activating PMS and the MoO₂/PMS system can effectively remove naphthalene derivatives in aqueous systems (Chen et al., 2021). CuMn₂O₄ nanoparticles were utilized to activate PMS for the degradation of crystal violet (Farajollahi et al., 2023). Recently, CuO as PMS activator has

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attracted much attention due to its abundant reserves, low price, simple preparation and high catalytic ability (Wei et al., 2022; Yan et al., 2021; Wang et al., 2021; Qin et al., 2020; Wang et al., 2019). Spongelike porous CuO exhibited good performance in activating PMS for the degradation of Acid Orange 7 (Qin et al., 2020). A series of metal oxides (ZnO, NiO, Al₂O₃, Fe₂O₃, MnO₂, CuO, CeO₂, La₂O₃) were synthesized by calcination method for PMS activation, and CuO showed a relatively higher performance in the degradation of 2, 6-dichlorophenol (Yan et al., 2021).

However, difficult recovery of CuO limited its application for PMS activation in aqueous systems. Therefore, the development of recyclable CuO-based heterogeneous catalysts is a meaningful thing. Due to the magnetic property, Fe₃O₄ was used as a support to obtain stable and magnetically recyclable heterogeneous catalysts (Li et al., 2023; Guo et al., 2023). Herein, CuO/Fe₃O₄ catalyst was prepared via a simple continuous precipitation method and used to activate PMS, which might simultaneously utilize the high catalytic property of CuO and the magnetic property of Fe₃O₄. The morphologies and properties of the CuO/Fe₃O₄ catalyst were systematically characterized by scanning electron microscopy (SEM), transmission electron microscopy (TEM), X-ray diffraction (XRD) and X-ray photoelectron spectroscopy (XPS). The catalytic performance of the CuO/Fe₃O₄ catalyst as PMS activator was evaluated through decomposing methyl blue (MB). Several influencing factors were investigated, such as initial pH, catalyst dosage, PMS concentration and reaction temperature. Furthermore, the applicability and stability of the CuO/Fe₃O₄ were also evaluated. In addition, the reactive oxygen species (ROS) generated in the CuO/Fe₃O₄/PMS were verified by the quenching experiment and EPR analysis.

2. Experimental section

2.1. Materials

Potassium peroxymonosulfate (PMS), Methylene blue (MB), Methyl Orange (MO), Tetracycline Hydrochloride (TC), isopropanol (IPA), *tert*-Butanol (TBA), L-Histidine (L-HIS), FeSO₄·7H₂O, CuSO₄·5H₂O, NaOH and HCl were obtained from Sinopharm Chemical Reagent Co., Ltd. All of the reagents and solvents used in the experiment were commercially obtained without any purification. Deionized water (DI water, 18.2 MΩcm) applied for preparing aqueous solutions.

2.2. Preparation of the catalysts

The Fe₃O₄ catalyst was fabricated using a simple method. Typically, 5.0 g FeSO₄·7H₂O was dissolved into 100 mL DI water under stirring. And pH value was adjusted to 12 using 1 mol/L NaOH solution. Then, the mixture was heated in a water bath at 70 °C for 2 h to obtain black precipitates of Fe₃O₄. The Fe₃O₄ precipitates were collected and cleaned with DI water and ethanol for four times each, followed by drying under vacuum at 70 °C.

The CuO/Fe₃O₄ catalysts were prepared as follows: 200 mg as-prepared Fe₃O₄ was uniformly mixed with 100 mL DI water with the aid of ultrasound, a certain amount of CuSO₄·5H₂O was added into the solution under stirring. After 1 h, pH value of the mixture was adjusted to 12 using 1 mol/L NaOH solution. Then, the mixture was heated in a water bath at 70 °C for 2 h to obtain CuO/Fe₃O₄ catalysts. The CuO/Fe₃O₄ precipitates were collected and cleaned with DI water and ethanol for four times each, followed by drying under vacuum at 70 °C. The molar ration of CuO to Fe₃O₄ were set to 2:1, 1:1, 1:2, respectively. And as-prepared catalyst were named as CuO/Fe₃O₄-2, CuO/Fe₃O₄-1, CuO/Fe₃O₄-0.5, respectively. If there is no special instruction, CuO/Fe₃O₄ appeared in the following section

was CuO/Fe₃O₄-1. The CuO catalyst was prepared by the same process without adding Fe₃O₄.

2.3. Material characterization

X-ray powder diffraction (XRD) pattern of samples were recorded on a powder X-ray diffractometer (D/max-2200/PC, Rigaku Corporation, Japan) with Cu Kα radiation, operating at 40 kV and 30 mA, where $\lambda = 0.15418$ nm for the Cu Kα line. XPS experiments were carried out on a RBD upgraded PHI-5000C ESCA system (Perkin-Elmer, USA), the shift of the binding energy due to relative surface charging was corrected using the C 1s level at 284.6 eV as an internal standard. The structure and morphology of the coatings were investigated by the field emission scanning electron microscopy (FESEM, FEI SIRION 200, FEI, USA). The structure and the morphology of the catalyst powders were observed by Transmission Electron Microscope (TEM, JEM-100CX, JEOL, Japan).

2.4. Experimental procedure

The catalytic activity of CuO/Fe₃O₄ was evaluated by degrading MB in the presence of PMS. Typically, 0.01 g CuO/Fe₃O₄ was added into 100 mL MB solution (20 mg/L) under stirring. After adsorption equilibrium for 30 min, PMS solution was added to trigger the oxidation process. Under continuous stirring, samples were taken at interval time, and immediately filtrated by a 0.22 μm syringe. The filtered fluid was instantly analyzed by a UV-vis spectrometer at 664 nm to measure the MB concentration. Each experiment was replicated three times.

3. Results and discussion

3.1. Characterization of catalysts

The morphologies of CuO, Fe₃O₄ and CuO/Fe₃O₄ were characterized by SEM (Figs. S1-S3). CuO owned sheet shape with a smooth surface (Fig. S1), and most Fe₃O₄ particles were agglomerated together due to the magnetic force (Fig. S2). CuO/Fe₃O₄ also exhibited sheet shape, but the surface is obvious rough, and the shape is irregular compared to CuO (Fig. S3). In addition, CuO/Fe₃O₄ also showed the sheet shape observed from the TEM images of CuO/Fe₃O₄ (Fig. 1a), and the lattice lines of CuO and Fe₃O₄ can be observed clearly in HR-TEM image (Fig. 1b). The lattice lines of 0.235 nm and 0.292 nm should be attributed to the (111) crystal plane of CuO and the (220) crystal plane of Fe₃O₄, respectively. Furthermore, the elemental mapping test was carried out to further determine the composition of CuO/Fe₃O₄. According to the results (Fig. S4), Cu, Fe and O elements coexisted in the catalyst, and dispersed uniformly on the composite surface.

XRD patterns of CuO, Fe₃O₄ and CuO/Fe₃O₄ were shown in Fig. 2. For Fe₃O₄, a series of diffraction peaks at 30.1°, 35.4°, 43.1°, 53.6° and 57.1° are observed distinctly, corresponding to the (220), (311), (400), (422) and (511) planes of the Fe₃O₄ (JCPDS PDF No. 65-3107). (Cui et al., 2021; Chen et al., 2021; Yang et al., 2016) For CuO, the major diffraction peaks appeared at 32.4°, 35.5°, 38.7°, 48.7°, 53.5° and 58.2°, which should be attributed to the (110), (-111), (111), (-202), (020) and (202) planes of monoclinic structure of CuO (JCPDS 48-1548) (Li and Wu, 2022). For CuO/Fe₃O₄, the characteristic peaks of both CuO and Fe₃O₄ were presented clearly, indicating the successful preparation of CuO/Fe₃O₄ composites.

The chemical state of CuO/Fe₃O₄ surface was investigated by XPS, as shown in Fig. 3. In Cu 2p XPS spectra, two peaks at near 933.1 eV and 953.2 eV are belong to Cu 2p_{3/2} and Cu 2p_{1/2}, respectively (Fig. 3a) And the other peaks at near can be assigned to the

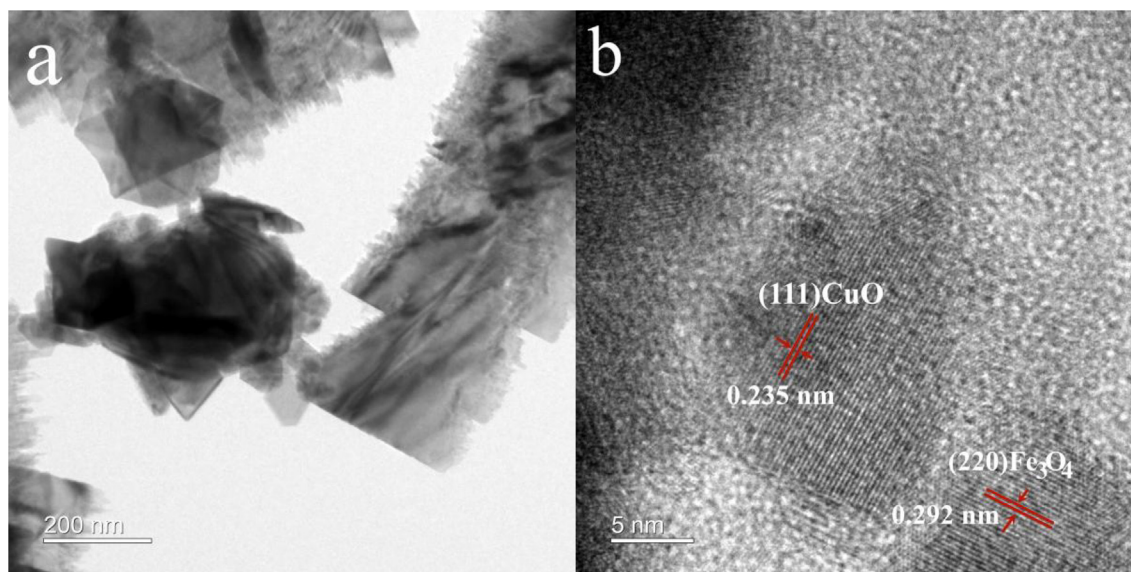


Fig. 1. TEM (a) and HR-TEM images (b) of CuO/Fe₃O₄ composites.

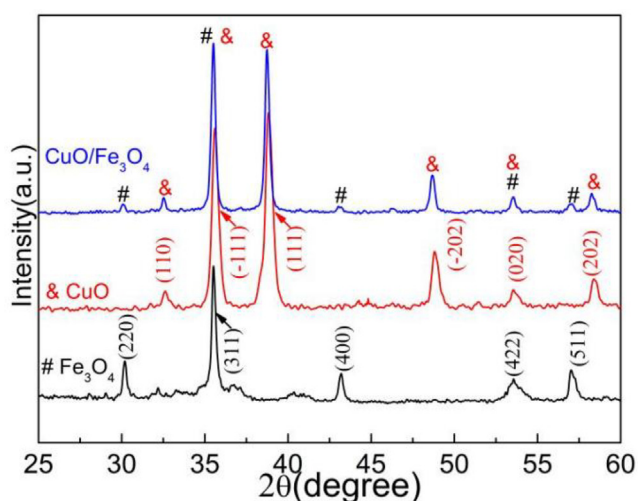


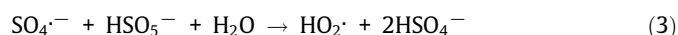
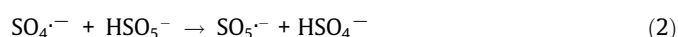
Fig. 2. XRD patterns of as-synthesized CuO, Fe₃O₄ and CuO/Fe₃O₄ composites.

satellite peaks of Cu 2p (Zuo et al., 2021; Xu et al., 2021). And the Auger peak at 568.73 eV further confirmed the presence of Cu²⁺ (Fig. 3b) (Zuo et al., 2021), indicating the existence of CuO rather than Cu₂O. The peaks of Fe 2p_{3/2} and Fe 2p_{1/2} of Fe₃O₄ at 711.7 eV and 723.8 eV with a satellite peak at 719.4 eV (Fig. 3c) (Cui et al., 2021; Singh et al., 2019). The peaks at near 529.8 eV and 531.4 eV in the O 1s spectra were attributed to the lattice oxygen and the adsorbed oxygen (Fig. 3d).

The catalytic performance of CuO/Fe₃O₄/PMS was explored by the degradation of MB. As shown in Fig. 4, the MB removal though the adsorption of CuO/Fe₃O₄ was negligible. The MB degradation by PMS without catalyst is no obvious. However, the CuO/Fe₃O₄/PMS system can realize the complete the MB degradation in 30 min. The results demonstrated that CuO/Fe₃O₄ can effectively activate PMS to decompose MB. Meanwhile, Fe₃O₄/PMS showed equally poor oxidation performance with a removal efficiency of only about 12% (Fig. S5). And the proportion of CuO in CuO/Fe₃O₄ composites is higher, the catalytic performance of CuO/Fe₃O₄/PMS is better for the degradation of MB. And all MB can be removed in 5 min by the CuO/PMS system (Fig. S5). Other studies

also have verified that Fe₃O₄ has a weak catalytic activity to active PS or PMS, which often needs external energy, such as ultrasonic sound, ultraviolet light (Yang et al., 2021). These results certified that the outstanding performance of CuO/Fe₃O₄ for PMS activation should be attributed to CuO. And the main role of Fe₃O₄ is to provide the magnetic property for CuO/Fe₃O₄ composites in our work, which is very convenient to recover the catalyst.

The effects of CuO/Fe₃O₄ dosage and PMS concentration on the MB removal were studied, as shown in Fig. 5. MB degradation efficiency drastically enhanced with the increased CuO/Fe₃O₄ dosage (Fig. 5a). When 0.1 g/L of catalyst is added into the solution, it needs 30 min to completely remove MB. As the catalyst amount is increased to 0.20 g/L, MB can be completely removed in 10 min. Subsequently, the degradation rate can be continuously improved by adding more CuO/Fe₃O₄ dosage (0.30 g/L). The result is mainly because the increased catalyst may provide more reactive sites for PMS activation (Yang et al., 2021; Zhao et al., 2021). As a result, more reactive species can be produced for the rapid decomposition of MB. The effect of PMS concentration was showed in Fig. 5b. Firstly, the degradation rate of MB increased with the increase of PMS concentration from 1 mmol/L to 2 mmol/L. As a strong oxidant, PMS can be activated on the reactive sites of catalyst to generate ROS. The reactive sites on the surface of CuO/Fe₃O₄ will be more fully utilized with the increase of PMS dosage. Consequently, more ROS can be produced to improve the removal efficiency of MB (Yang et al., 2021). However, the degradation rate of MB decreased later with the increase of PMS concentration from 2 mmol/L to 3 mmol/L. Excessive PMS can cause the self-quenching reactions of PMS (Liu et al., 2021; Ma et al., 2018). As described in Eqs. (1)–(3), excessive PMS will promote the conversion of ·OH and SO₄^{·-} to SO₅^{·-} and ·HO₂ with lower reactivity (Zhao et al., 2021; Liu et al., 2021).



The pH value of the solution not only influences the existence form of PMS, but also the properties of the catalyst (Liu et al., 2023). So it is very important for the catalytic activity of the

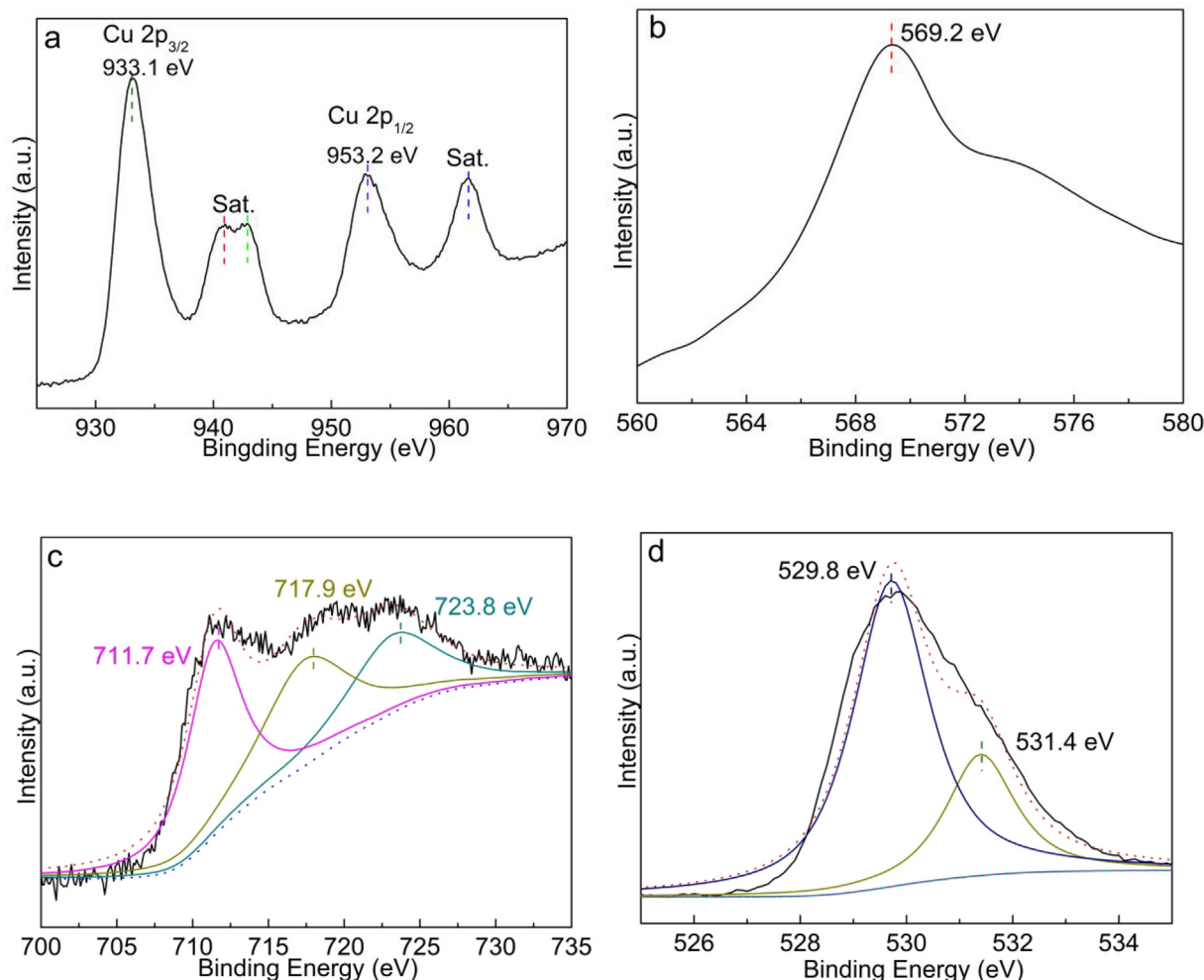


Fig. 3. XPS spectra of Cu 2p (a), Cu LMM (b), Fe 2p (c) and O 1s (d) of CuO/Fe₃O₄ composites.

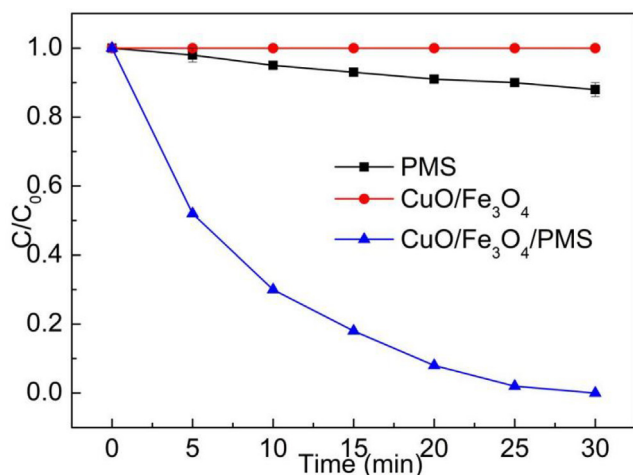


Fig. 4. Degradation of MB in various systems. Initial conditions: [MB] = 20 mg/L, [PMS] = 1 mmol/L, [CuO/Fe₃O₄] = 0.1 g/L, pH = 7.55.

CuO/Fe₃O₄/PMS system. To test the effect of initial pH on the MB degradation, different initial pH of solution was adjusted by adding 1 mol/L NaOH solution or 1 mol/L HCl solution. As presented in Fig. 6a, the removal efficiencies of MB were 14.1%, 63.3%, 100% and 85.2% in 30 min at pH 2.21, 4.40, 7.55 and 12.10, respectively.

Meanwhile, as showed in Fig. S6, the MB removal basically followed the first order kinetic model (Eq. (4)), where C and C₀ represented the MB real-time and initial concentration, respectively, k_{obs} was the rate constant. Observed from Fig. 6b, the highest k_{obs} was acquired at a neutral pH (pH = 7.55).

$$\ln(C/C_0) = -k_{\text{obs}}t \quad (4)$$

In most cases, the highest degradation rate of pollutants via PMS/catalyst system is obtained under near-neutral conditions (Liu et al., 2023; Li and Wu, 2022; Zhen et al., 2021). Under acidic conditions, strong hydrogen bonds will be formed between excess H⁺ with O-O in PMS, which inhibit the reaction between catalysts and PMS. Thus it depresses the formation of ROS, and further reduce the degradation of pollutant. Besides, metal ions from metal oxides are easy to dissolve into the reaction solution under acidic conditions. But the leaching ions always have a weaker ability for PMS activation. In our work, the extreme acidic condition (pH = 2.21) is bad for PMS activation by CuO/Fe₃O₄ composites. And the MB removal efficiency was very tiny (14.1%). Similar phenomenon was displayed in our previous work, the MB degradation in the CuO/PMS system was negligible under extreme acidic condition (pH ≈ 2) (Li and Wu, 2022). On the other hand, although the increasing of OH⁻ ions may accelerate PMS decomposition, the MB removal decreased from 100% at pH = 7.55 to 85.2% at pH = 12.10. The several reasons may lead to this result. Firstly, the pK_{a2} of PMS is 9.4, so PMS mainly exists in the form of SO₅²⁻

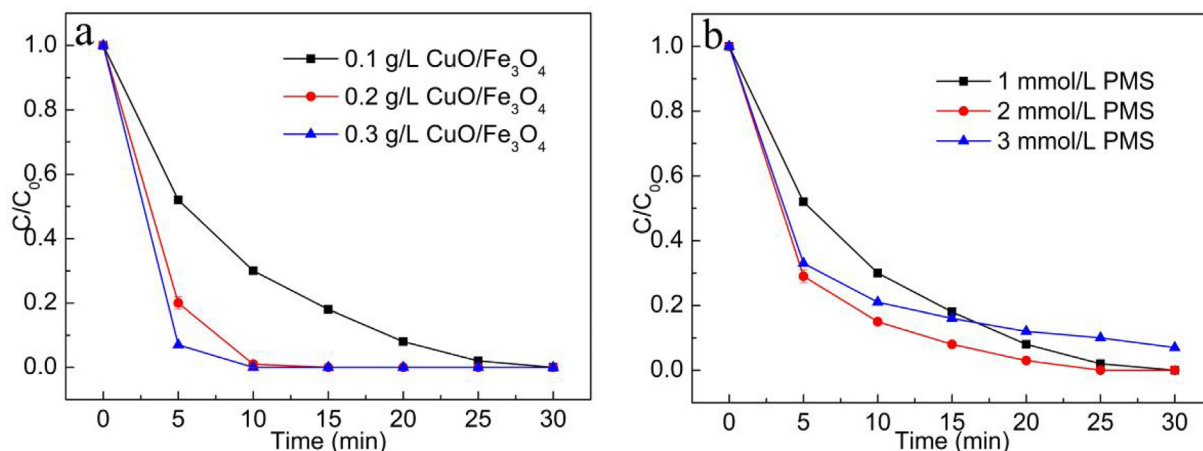


Fig. 5. The effect of CuO/Fe₃O₄ loading (a) and PMS concentration (b) on MB degradation. Initial conditions: [MB] = 20 mg/L, [PMS] = 1 mmol/L, [CuO/Fe₃O₄] = 0.1 g/L, pH = 7.55.

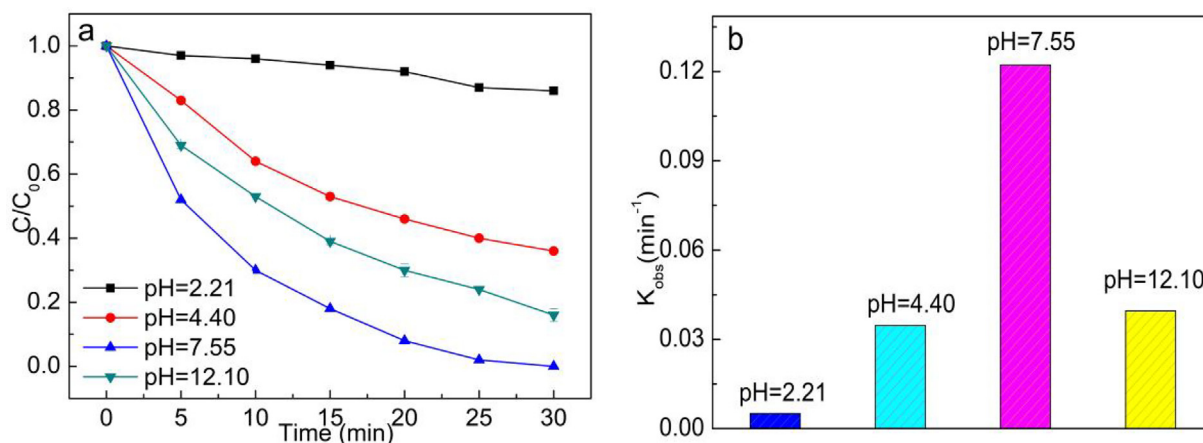
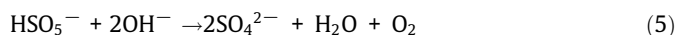


Fig. 6. The effect of initial pH value on MB removal (b) and degradation rates of MB in the CuO/Fe₃O₄/PMS system. Initial conditions: [MB] = 20 mg/L, [PMS] = 1 mmol/L, [CuO/Fe₃O₄] = 0.1 g/L.

under strongly alkaline conditions (pH = 12.10). The isoelectric point (pH_{pzc}) of the CuO/Fe₃O₄ composite was about pH 8.8 (Zhen et al., 2021; Ding et al., 2020). Therefore, the surface of CuO/Fe₃O₄ catalyst was negative under strongly alkaline conditions (pH = 12.10). Consequently, electrostatic repulsive forces are generated between PMS components and catalysts under strongly alkaline conditions (pH = 12.10), preventing the generation of ROS. Secondly, inactive materials such as SO₄²⁻ will be formed through the hydrolysis of PMS under basic conditions (Eq. (5)) (Rastogi et al., 2009). In addition, SO₄^{·-} was easily converted to ·OH under alkaline conditions (Eq. (6)), which had lower oxidation capacity and selectivity (Liu et al., 2023).



The operating temperature also affect the chemical reaction. Here the PMS activation at varying temperatures with/without CuO/Fe₃O₄ composites toward MB oxidation were comprehensively investigated. As presented in Fig. 7a, MB molecules can be degraded through thermally activated PMS without catalyst. The MB degradation rate was improved with the increase of reaction temperature. It was improved from 12.1% to 33.9% with increasing

reaction temperature from 20 to 40 °C. PMS can be activated by energy, and a higher reaction temperature can supply more energy to promote the decomposition of PMS into more ROS (Duan et al., 2018), resulting in the higher degradation of MB. Compared with the thermally activated PMS, the MB decomposition by PMS activation in the presence of CuO/Fe₃O₄ composites was greatly improved (Fig. 7a). Similarly, the catalytic activity was also enhanced with the increasing reaction temperature. It took 25 min to completely degrade MB at 20 °C, while 10 min at 40 °C. According to the first order kinetic model (Fig. S7), the rate constants were obtained. The rate constant is increased from 0.1223 min⁻¹ at 20 °C to 0.3501 min⁻¹ at 40 °C (Fig. S8). The molecular movement would be accelerated with the increase of temperature, the higher temperature may facilitate the mass transfer process of heterogeneous systems (Duan et al., 2018; Yu et al., 2022; Asif et al., 2021). In a word, the upper temperature is good for the MB degradation based on the above-mentioned reasons. In addition, the activation energy of this reaction measured by employing the Arrhenius equation (Eq. (7)) (Qin et al., 2020; Ma et al., 2018), where R is the molar gas constant (8.314472 J/(mol·K)), T is the temperature (K), k_{obs} was the rate constant. The curve between 1/T and ln k_{obs} was plotted (Fig. 7b), and calculated Ea value is about 40.34 kJ/mol. The Ea value is lower than those of reported PMS-based systems, such as Co₃O₄-Bi₂O₃/PMS (50.5 kJ/

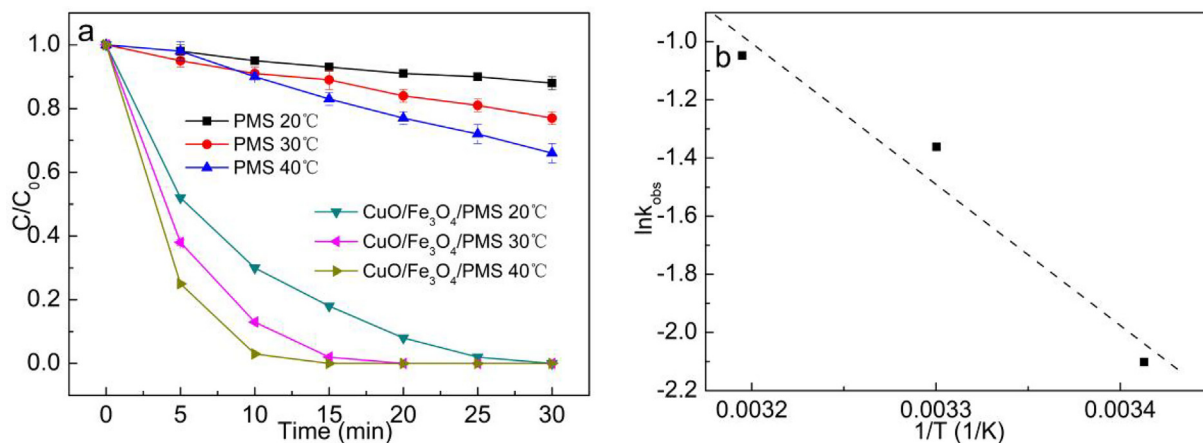


Fig. 7. The effect of reaction temperature on degradation rates of MB (a), and fitting of activation energy for CuO/Fe₃O₄/PMS system. Initial conditions: [MB] = 20 mg/L, [PMS] = 1 mmol/L, [CuO/Fe₃O₄] = 0.1 g/L, pH = 7.55.

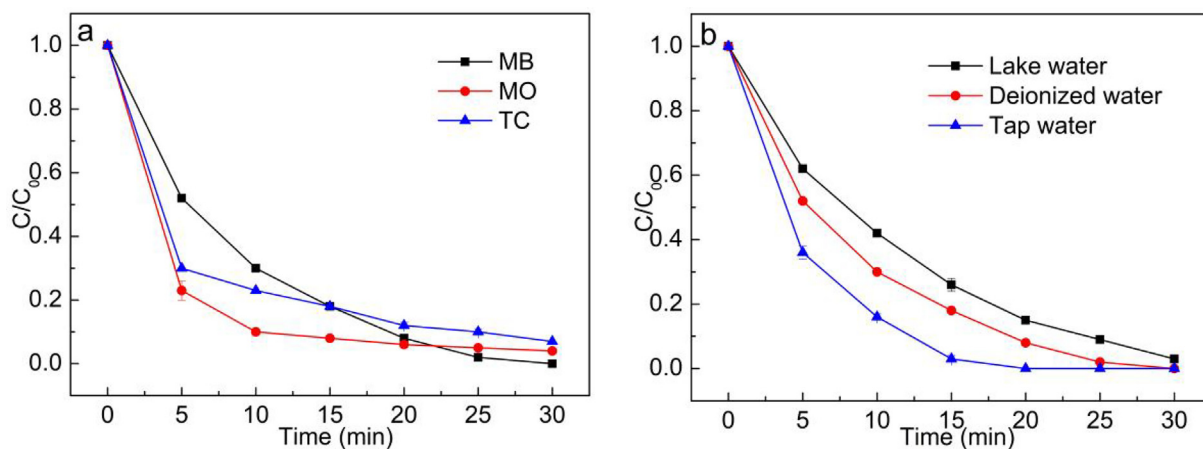


Fig. 8. Degradation of different pollutants in CuO/Fe₃O₄/PMS system (a), the effect of water bodies on MB degradation in CuO/Fe₃O₄/PMS system (b). Initial conditions: [MB/MO/TC] = 20 mg/L, [PMS] = 1 mmol/L, [CuO/Fe₃O₄] = 0.1 g/L, pH = 7.55.

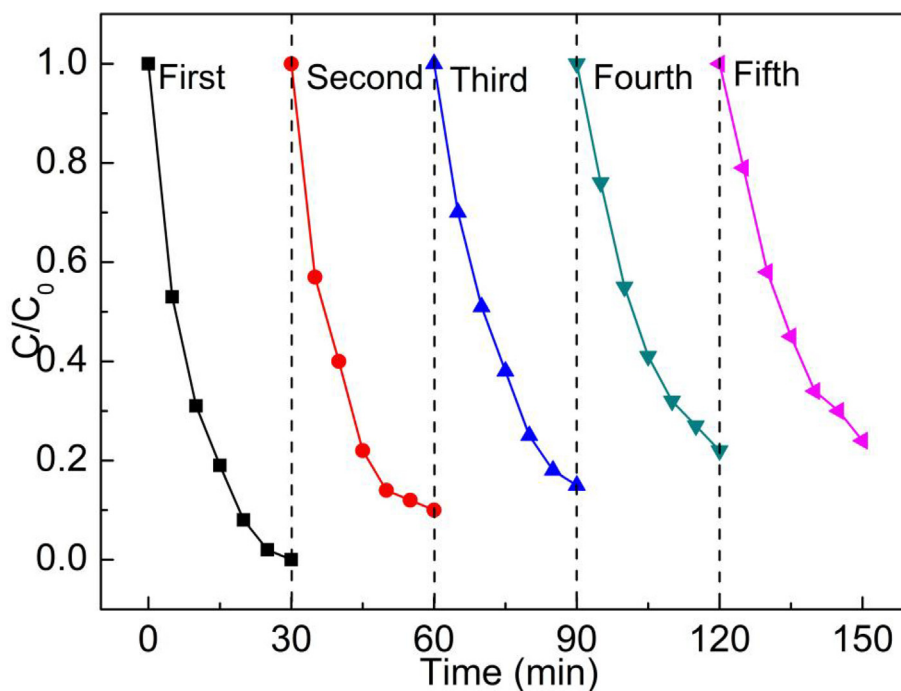


Fig. 9. Cycling tests of CuO/Fe₃O₄/PMS system toward MB degradation. Initial conditions: [MB] = 20 mg/L, [PMS] = 1 mmol/L, [CuO/Fe₃O₄] = 0.1 g/L, pH = 7.55.

mol), CoMnAl-metal oxides/PMS (76.8 kJ/mol) and N-rGO/PMS (46.9 kJ/mol), indicating that the catalytic oxidation process in the CuO/Fe₃O₄/PMS system could be easily achieved (Qin et al., 2020).

$$\ln k_{\text{obs}} = \ln A - E_a/RT \quad (7)$$

To examine the wide applicability of this technology, the removal efficiencies of various organic pollutants and MB degradation efficiencies in different water bodies were explored respectively. Water bodies include tap water from our lab and lake water from the artificial lake on campus. MB, MO and TC were used as various organic pollutants. Details about the related process were described in the Supporting Information (Text S1 and Text S2). Fig. 8a presented the removal efficiencies of various organic pollutants in the CuO/Fe₃O₄/PMS system. Different pollutants have different molecular constructions and physicochemical characteristics, some differences in degradation efficiencies between pollutants are observed in the CuO/Fe₃O₄/PMS system. But all pollutants can be degraded effectively in CuO/Fe₃O₄/PMS system (Fig. S9). Surprisingly, it only took 10 min to degrade most of MO. Fig. 8b exhibited MB degradation efficiencies in different water matrices. Clearly, the removal efficiencies of MB in different water matrices all are nearly 100% (Fig. S10). The apparent rate constants for MB degradation were calculated by the pseudo first order kinetic model (Fig. S11). The k_{obs} values for MB degradation were 0.2266, 0.1468 and 0.1101 min⁻¹ in TW, DW and LW, respectively (Fig. S12). What's more, the existence of positive ions in the MB solution, such as K⁺, Ca²⁺, Na⁺, Mg²⁺, had no inhibition for the removal of pollutants by the CuO/Fe₃O₄/PMS system (Fig. S13), other researches had got the similar phenomenons (Zhang et al., 2023; Zhong et al., 2022).

The stability and reusability of CuO/Fe₃O₄ composites were evaluated via cyclic experiment, which are very important for practical application. After each cycle, the used catalyst was collected by an external magnet (Fig. S14), and reused after drying. Details about the related process were described in the Supporting Information (Text S3). Observed from Fig. 9, the MB degradation efficiency was depressed along with the increase of number of cycle. The main reason should be that the pollutants adsorbed on the surface of CuO/Fe₃O₄ composites gradually accumulated each cycle, thereby hindering the interaction between CuO/Fe₃O₄ composites and PMS molecules to produce ROS (Yang et al., 2021). Satisfactorily, the MB degradation efficiency still remained 77.48% after five runs. Meanwhile, the XRD pattern of CuO/Fe₃O₄ composites has no remarkable change (Fig. S15). The results demonstrated that CuO/Fe₃O₄ composites have good stability and reusability, highlighting the practicability in water remediation.

To determine the species of generated ROS for the MB degradation, a quenching experiment was carried out in CuO/Fe₃O₄/PMS system. Isopropanol (IPA), *tert*-butyl alcohol (TBA) and L-histidine (L-HIS) were used as quenching reagents. TBA is a commonly used to quench ·OH, and IPA can synchronously quench ·OH and SO₄⁻ (Wang et al., 2021). In addition, ·OH, SO₄⁻ and ¹O₂ all can be quenched by L-histidine, the k values are $5.0 \times 10^9 \text{ M}^{-1}\text{s}^{-1}$, $2.5 \times 10^9 \text{ M}^{-1}\text{s}^{-1}$ and $1.5 \times 10^8 \text{ M}^{-1}\text{s}^{-1}$ for ·OH and SO₄⁻ and ¹O₂, respectively (Li et al., 2022). As depicted in Fig. 10a, the degradation efficiency of MB was slightly depressed in the CuO/Fe₃O₄/PMS system by adding TBA. When IPA and L-HIS were added into the system, the MB removal efficiency were reduced to 77.8% and 16.8%, respectively. According to the pseudo first order kinetic model (Fig. 10b), the calculated k_{obs} values were decreased from 0.1223 min⁻¹ without quenching reagents to 0.1017, 0.0502, 0.0044 min⁻¹ in the presence of TBA, IPA, L-HIS, respectively

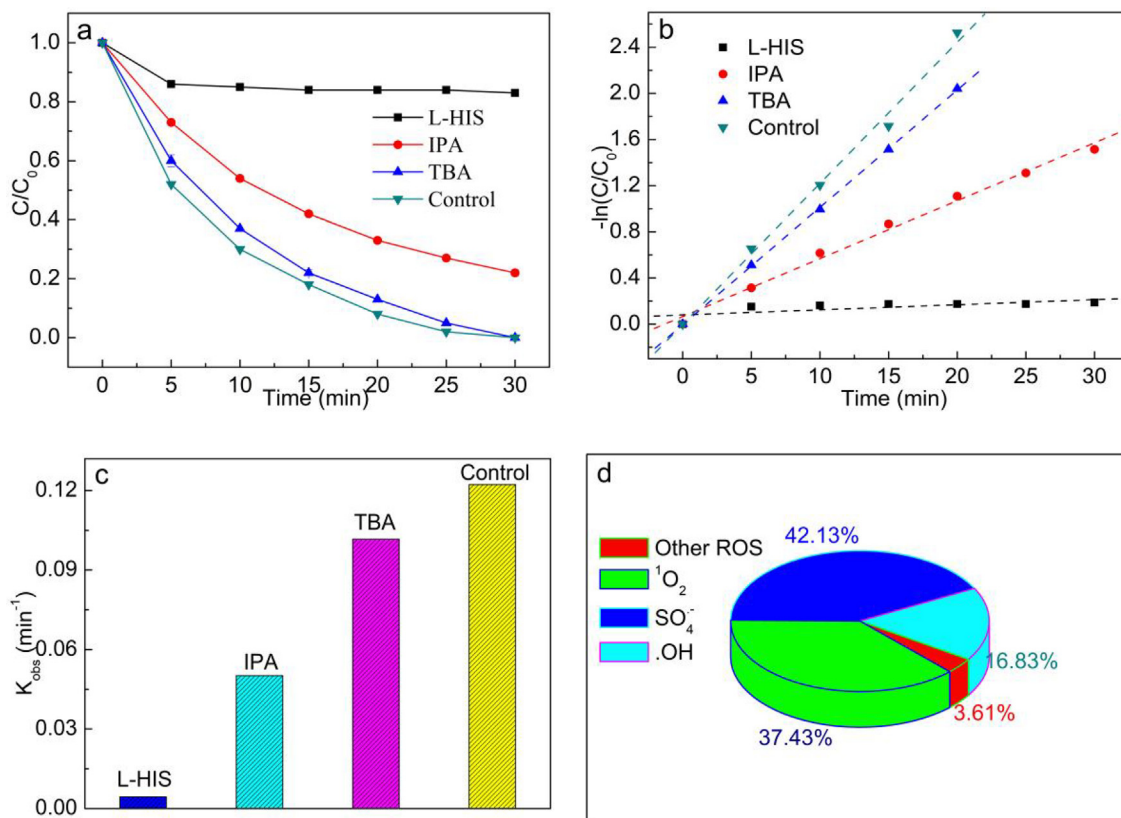


Fig. 10. MB degradation (a), pseudo-first-order kinetic curves for MB degradation (b) and MB degradation rate constants (c) in CuO/Fe₃O₄/PMS system in the presence of different scavengers. The contribution of ·OH, SO₄⁻, ¹O₂ and other ROS in CuO/Fe₃O₄/PMS system (d). Initial conditions: [MB] = 20 mg/L, [PMS] = 1 mmol/L, [CuO/Fe₃O₄] = 0.1 g/L, pH = 7.55, [IPA] = [TBA] = 50 mmol/L, [L-histidine] = 10 mmol/L.

(Fig. 10c). The k values of different quenching experiments were adopted for estimation of ROS contribution. The different ROS contributions were evaluated via Eqs. (8)–(11), where the k_0 represents the pristine rate constant in CuO/Fe₃O₄/PMS system, k_1 , k_2 , and k_3 were the kinetic constants of MB degradation with the addition of TBA, MeOH, and L-histidine, separately (Yu et al., 2022; Wang et al., 2020; Zhou et al., 2020). The results were presented in Fig. 10d. The results indicated that $\cdot\text{OH}$; $\text{SO}_4^{\cdot-}$ and $^1\text{O}_2$ all participated in the process, $\text{SO}_4^{\cdot-}$ and $^1\text{O}_2$ played the dominant role. And the ROS were further detected via EPR tests in CuO/Fe₃O₄/PMS system. As shown in Fig. 11, both signals of DMPO- $\cdot\text{OH}$, DMPO- $\text{SO}_4^{\cdot-}$ and TEMP- $^1\text{O}_2$ were observed in CuO/Fe₃O₄/PMS system (Yu et al., 2022; Li et al., 2022; Ouyang et al., 2022).

$$\lambda(\cdot\text{OH}) = (k_0 - k_1)/k_0 \quad (8)$$

$$\lambda(\text{SO}_4^{\cdot-}) = (k_1 - k_2)/k \quad (9)$$

$$\lambda(^1\text{O}_2) = (k_2 - k_3)/k_0 \quad (10)$$

$$\lambda(\text{other ROS}) = k_3/k_0 \quad (11)$$

According to these results and some previously reported results (Yan et al., 2021; Zuo et al., 2021; Li et al., 2020; Li et al., 2019; Lei et al., 2015); the possible catalytic mechanism is illustrated in Fig. 12. Meanwhile, considering the dominant role of CuO in the CuO/Fe₃O₄ composites for PMS activation, the main reactions of producing ROS in the CuO/Fe₃O₄/PMS system were depicted as Eqs. (12)–(15). $\equiv\text{Cu(II)}$ on the surface of CuO reacted with PMS to generate $\equiv\text{Cu(III)}$ and $\text{SO}_4^{\cdot-}$ (Eq. (12)). The generated $\equiv\text{Cu(III)}$ reacted with PMS to form $\text{SO}_5^{\cdot-}$ (Eq. (13)). In addition, the generated $\text{SO}_5^{\cdot-}$ can interact with H₂O to produce $\cdot\text{OH}$ (Eq. (15)), the self-reaction of $\text{SO}_5^{\cdot-}$ will form $^1\text{O}_2$ (Eq. (16)). Subsequently, these ROS decomposed MB molecules into intermediates and mineralization products (CO₂ and H₂O) (Eq. (16)).

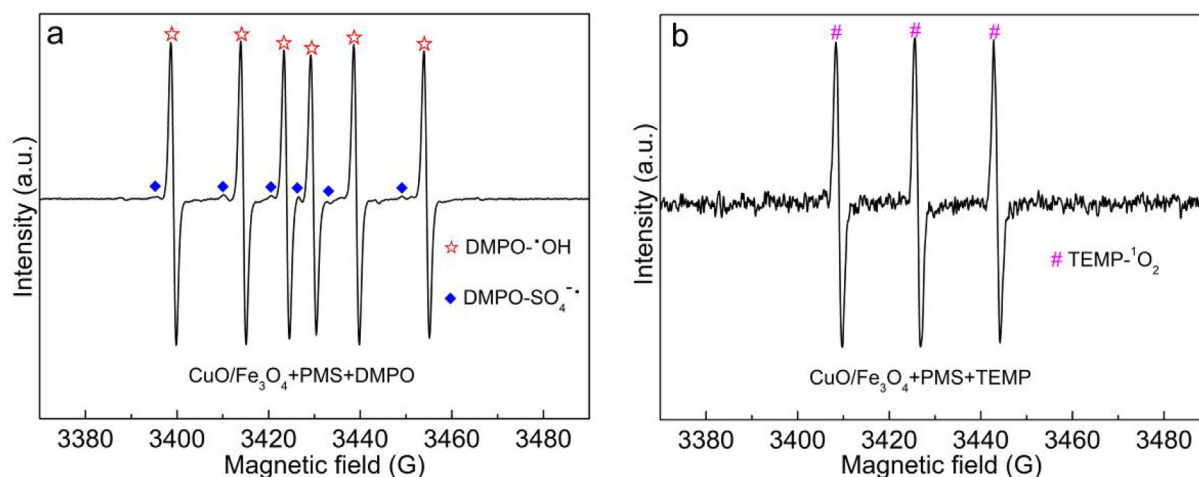


Fig. 11. EPR spectra of $\cdot\text{OH}$ and $\text{SO}_4^{\cdot-}$ (a) and $^1\text{O}_2$ (b) in CuO/Fe₃O₄/PMS system.

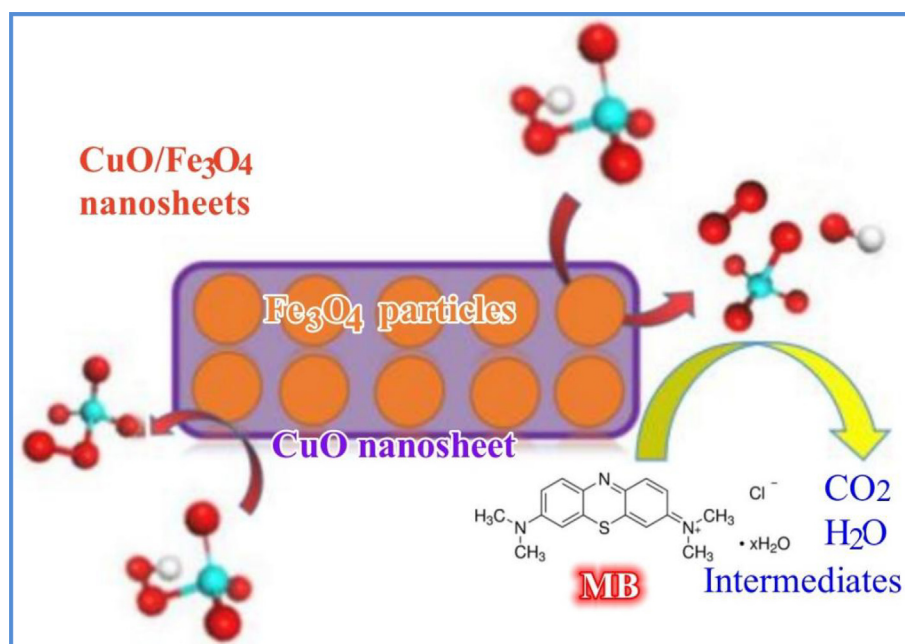
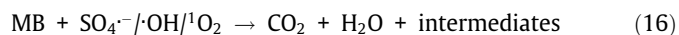
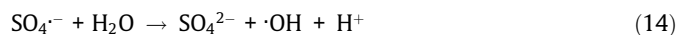
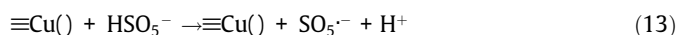
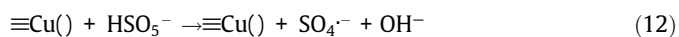


Fig. 12. Possible mechanism of MB degradation in the CuO/Fe₃O₄/PMS system.



4. Conclusion

In summary, magnetic CuO/Fe₃O₄ nanosheets were facilely synthesized for PMS activation to achieve high-efficient degradation of organic pollutants. CuO/Fe₃O₄ showed the good catalytic performance in a wide pH range (4–12). Higher dosages of CuO/Fe₃O₄, appropriate PMS concentration, higher reaction temperature and the neutral solution pH value were beneficial for MB removal. The radical quenching test and ESR showed that ·OH, SO₄^{·-} and ¹O₂ were generated in the CuO/Fe₃O₄/PMS system, and SO₄^{·-} and ¹O₂ played the main role. In addition, CuO/Fe₃O₄ could be collected by magnetic separation and reused with good performance. Moreover, other organic pollutants can be degraded completely in CuO/Fe₃O₄/PMS system, and CuO/Fe₃O₄/PMS system exhibited satisfactory removal of MB in real water matrix. In a word, high removal efficiency, the stability, reusability and wide applicability of CuO/Fe₃O₄/PMS were good for its utilization in the environmental remediation.

CRedit authorship contribution statement

Deyong Wu: Conceptualization, Methodology, Writing – original draft, Writing – review & editing. **Xiangfei Li:** Methodology, Investigation.

Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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Appendix A. Supplementary material

Supplementary data to this article can be found online at <https://doi.org/10.1016/j.arabjc.2023.105285>.

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